phosphoinositides are quite well separated, but cephalin is distributed between the two fractions. Thus in present work when commercial crude phosphatides were extracted five times with a total of 6.5 ml. of isopropyl alcohol per gram, the combined extracts contained 61% acetone-soluble material, 23.2% lecithin, and 10.6% cephalin. Practically all the inositolcontaining material and 77% of the sugar remained in the insoluble fraction.

It is obvious that the separation between oil and phosphatide components achieved by acetone extraction followed by isopropyl alcohol or ethyl alcohol cannot be obtained by the use of isopropyl alcohol alone; but the direct extraction with isopropyl alcohol gives a good separation of the inositol containing fraction from the other components and, in addition, uses a much smaller volume of solvents. If it is desirable, the oil may later be removed from the soluble portion by acetone in the usual way.

While five extractions and a total of 6.5 ml. of isopropyl alcohol per gram of phosphatides were used in this work, for some purposes a less complete extraction may be satisfactory. For example, by extracting only two times with a total of 2.5 ml. isopropyl alcohol per gram 40.8% of the crude phosphatides would be extracted as indicated by the data in Table I. This extract would contain 34% acetone-insoluble material and the remainder would be mainly oil. The fraction remaining after the isopropyl alcohol extraction would contain 91.8% acetone-insoluble material.

Separations of lecithin from cephalin in the soluble portion and of the phosphoinositides of the insoluble portion have been accomplished as yet only by methods suitable for small-scale laboratory purposes. However, current reports indicate that commercial fractionations of soybean phosphatides are following closely upon knowledge of composition and laboratory separations and that further developments depend upon the growth of more fundamental information.

Summary

Isopropyl alcohol has many advantages as a commercial solvent and gives useful separations of soybean phosphatides. When commercial crude phosphatides were extracted five times with a total of 6.5 ml. isopropyl alcohol per gram, 31.5% oil, 12% lecithin, and 5.5% cephalin were dissolved. Practically all the inositol-containing material and about 77% of the sugars remained insoluble. Further extractions with ethyl alcohol removed the remaining lecithin together with additional cephalin.

After removal of the oil from the crude phosphatides with acetone, the extraction of the isopropyl alcohol-soluble material required twice the amount of isopropyl alcohol used for the direct extraction described above.

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Variations in the Chemical, Physical, and Organoleptic Properties of Soybean Oil Hydrogenated Under Widely Varying Conditions

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T is generally accepted that there is a relationship between the flavor stability of soybean oil and its oxidative stability. Consequently many workers in the field subscribe to the assumption that the flavor deterioration of fats is due to an autooxidative process of some type involving the polyunsaturated glycerides (1, 2).

In the work to be reported here soybean oil was hydrogenated to various degrees of hardness under a variety of conditions so as to produce fats of widely varying oxidative stability. No correlation was observed between flavor scores of fresh or aged products and their oxidative stabilities as measured by the active oxygen method (3, 4). Furthermore the content of polyunsaturated glycerides appeared to bear no relationship to flavor stability.

As reported by other workers (5), at moderate pressure chemical selectivity was found to vary directly with catalyst concentration and with temperature up to 200°C., and inversely with hydrogen pressure and rate of agitation. But at hydrogen pressures over 500 psi. the effect of changes in catalyst concentration and agitator speed was reversed. That is, selectivity then varied inversely with catalyst concentration and directly with agitator speed.

The percentage of high-melting trans isomers formed during hydrogenation (6) is also a function of pressure and varies inversely with it. Yet higher melting products were obtained, for a given drop in refractive index, when higher pressures were used. Apparently the amount of fully saturated glycerides

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		Hydroger	nation Conditions			Meltin	g Point	Soften-	Tino	Time	:	A O M		Tuene
Sample No.	Hydro- gen (psi.)	Temp. (° 0.)	Nickel Catalyst (%)	Time (Min.)	R.I.ª	F.A.C. (°C.)	Wiley (°C.)	ing Point (°C.)	leic (%) °	lenic (%)°	Diene (%)°	Stability (hours)	Flavor Score	Acids (%)
Original Oil					51.3				55.6	8.0	0.44			
_ 1	10	200	H	170	40.5	103	101	100	0.18	0.008	0.24		2	
2	225	200	ч	30	40.5	104	102	101	0.02	0,00	0.21		9	
3	950	200-250	н	01	39.7	114	112	110	0.04	0.00	0.23		4	
4	10	200	1	240	41.8	96	96	93	1.28	0.00	0.50	215	6.5	54
2	225	195-205	0.05	38	41.6	118	104	98	5.37	0.13	0.32	115	90	44
9	100	200-225	0.05	ŝ	42.1	122	123	109	12.30	0.64	0.46	70	7	30
7	600	200		135	41.7	125	119	114	7.37	0.29	0.44		9	
- 00	500	200-205	0.05	e9	46.3	81	Too soft	Too soft	28.76	2,53	0.71		7.5	
6	10	200	0.25	165	46.3	Too soft	Too soft	Too soft	21.80	0.90	3.43		œ	
10	400	198-205		5	45.9	98	87	Too soft	28.59	1.39	1.18		8.5	
11	400	125	1	30	45.8	98	87	Too soft	28.31	1.34	0.33		8.5	
* Refractive indices at 60°C	. using a Bı	utyro refracton	neter.		1									

° Polyunsaturated by the A.O.C.S. Tentative Method Cd. 7-48.

	A.0.M.	b) Stabil- Flavor Actuals (%) ity Score (%)	84 84 29 29 20 20 20 20 20 20 8 20 8 20 8 20	48 35 8 18.0 26 35 8 18.0 26 35 8 19.3 79 35 7 25.1 35 45 7 25.1 35 50 7 35.8 31 50 7 35.8	
	T	lenic Di (%) ° (%)	7.49 3.53 3.53 1.96 2.58 2.19 2.58 2.11 2.58 2.11 2.58 2.11 2.58 2.11 2.58 2.11 2.58 2.11 2.58 2.11 2.58 2.11 2.58 2.11 2.58 2.11 2.58 2.11 2.58 2.11 2.58 2.58 2.58 2.58 2.58 2.58 2.58 2.58	2.269 2.469 2.846 2.846 2.846 2.946 2.11 2.24 2.11 2.00 2.00 2.00 2.00 2.00 2.00 2.00	
ABLE III		leic (%) °	53.65 28.61 28.96 29.46 34.97	51,89 28.40 27.81 25.30 21.26	
	Soften- ing Point (°C.)		87 87 101 Too soft Too soft	115 111 106 Too soft Too soft	
	ng Point	Wiley (°C.)	Too soft 119 Too soft Too soft	130 123 118 118 83 83	
	Meltir	F.A.C. (°C.)	108 131 Too soft Too soft	135 135 123 Too soft 83	
ТА	R. I.a		51.3 46.6 46.6 46.7	72444444 17244444 172757 17275 17755 17275 17275 17275 177555 177555 177555 177555 1775555 177555 177555 177	
		Time	2 hr., 30 min. 30 sec. 33 min.	30 sec. 45 sec. 80 sec. 7 min., 45 sec. 57 min.	
	nation Conditions	Nickel Catalyst (%)	None added 0.01 0.1 0.01	0.0000 0.000 0.000 0.000 0.000	meter. Jd. 7-48.
	Hydroge	Temp. (°C.)	225-250 225-250 225 225	200-230 200-230 200-215 200 200 200	tyro refracto tive Method (
		Hydro- gen (psi.)	1800 1250 30 30	1100 550 225 30	using a Bu D.C.S. Tentai
	Sample No.		Original Oil. 12 14	Original Oil 16 17 18 19 20	 Refractive indices at 60°C. Polyunsaturated by the A.(

Conj. Diene (%)° 0.48 1.048 0.052 0.94 0.65 0.94 0.65 0.65 Lino-lenic (%)° 22.22.22 22.22 22.22 24.25 24.25 25.22 25.23 25.25 25. Lino-leic (%)° 51.89 221.64 27.81 18.07 18.07 18.07 17.99 15.87 15.07 15.07 15.07 21.7 Softening Point (°C.) Too soft Too soft 111 108 108 108 Too soft 121 131 Too soft 123 122 122 122 87 135 Wiley (°C.) Melting Point F.A.C. (°C.) Iodine Value^b $100.5 \\ 102.3$ 106.3 R. I.a 0.0044444 0.0074444 0.007445 0.00446 0.00446 0.006 TABLE IV 8 min. 10 min. 45 sec. 66 min. 28 min. 70 min. 9 min. Time Agitator rpm. 11140 11140 11140 11140 11140 11140 11140 11140 11140 Hydrogenation Conditions Nickel Catalyst (%) 1 0.05 0.05 0.05 0.05 0.05 225 150-165 200-230 200-205 200-205 200-205 200-205 200-205 200-205 200-205 Temp. (°C.) Hydrogen (psi.) Original Oil 21. 23. 23. 23. 23. 26. 26. 29. 29. Sample No.

rather than the amount of trans acids determined the final consistency of these fats.

Extent of Hydrogenation

Experiments on the relationship between flavor stability and extent of hydrogenation were done, using a carbon-steel, gas-fired converter of 5-l. capacity equipped with a mechanical agitator. A 3,500-g. charge of refined and bleached soybean oil was hardened at 200°C. and 30 psi. with 0.2% by weight of a commercial reduced nickel catalyst (containing about 25% Ni). At intervals, as indicated in Table I, 500-g. samples were withdrawn into an evacuated flask and allowed to cool to 80°C. before admitting air. Each was filtered with bleaching clay and filter aid until the filtrates gave no discoloration with boiling ammonium polysulfide solution.

The oils of each series were then deodorizeed concurrently for five hours at 200°C. and 1-mm. pressure in 1-l. glass laboratory deodorizers. Each was stabilized with 0.005% citric acid and then cooled. Then the freshly deodorized oils were graded by a flavor panel, using the scoring system developed at the Northern Regional Research Laboratory (7). Samples were aged in covered glass jars at 60°C. for three days and then graded again. This procedure was repeated four times (Series 1-4 of Table I), using a different lot of soybean oil each time.

TABLE I

			Ser	ies 1				
	Time A O M Flavor Panel Score						core	
(min.)		R.1.*	(hours)		Fresh	Fresh Aged (3 60°C		
$\begin{array}{c} 0\\ 3\\ 6\\ 9\\ 24\\ 49 \end{array}$		$51.1 \\ 47.5 \\ 43.9 \\ 42.2 \\ 40.2 \\ 38.4$	28 40 60 110 37 Over	5)) 5 400	9 9 9 9 9 9 9		6 6 7 6 7.5 7	
			Ser	ies 2				
				C1 0		Flavor Panel Sco		
Time (min.)	R. I.ª	Iodine Value ^b	Lino- leic	Lino- lenic	Conj. Diene	Fresh	Aged (3 days, 60°C.)	
$\begin{array}{c} 0 \\ 4 \\ 7 \\ 11 \\ 17 \\ 31 \end{array}$	50.8 47.0 43.6 41.1 39.6 37.5	$ \begin{array}{r} 132.1\\107.3\\89.7\\73.4\\63.9\\49.6\end{array} $	53.4 25.2 9.9 1.8 0.26 0.01	$\begin{array}{r} 8.40 \\ 2.60 \\ 0.50 \\ 0.03 \\ 0.00 \\ 0.00 \end{array}$	$\begin{array}{c} 0.30 \\ 1.24 \\ 0.63 \\ 0.28 \\ 0.14 \\ 0.12 \end{array}$	9 9 9 9.5 9	6 5 7.5 7.5 7.5 7	
			Ser	ies 3				
$ \begin{array}{c} 0 \\ 3 \\ 5 \\ 8 \\ 13 \\ 28 \end{array} $	$51.2 \\ 46.7 \\ 43.8 \\ 41.5 \\ 40.2 \\ 38.0$	$\begin{array}{c c} 132.9\\ 105.1\\ 87.4\\ 76.4\\ 66.5\\ 52.6\end{array}$	$\begin{array}{r} 48.7 \\ 27.0 \\ 11.9 \\ 2.7 \\ 0.2 \\ 0.00 \end{array}$	$\begin{array}{r} 8.12 \\ 2.70 \\ 0.65 \\ 0.04 \\ 0.03 \\ 0.00 \end{array}$	$\begin{array}{c} 0.31 \\ 0.81 \\ 0.37 \\ 0.24 \\ 0.12 \\ 0.09 \end{array}$	9 9 9 9 9 9	6 5 6 7 7	
			Ser	ies 4				
$0\\3\\5\\8\\12\\24$	51.2 46.5 43.1 41.1 39.7 37.5	$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	$55.6 \\ 27.6 \\ 10.4 \\ 2.9 \\ 0.3 \\ 0.0 $	$\begin{array}{c} 8.0 \\ 2.6 \\ 0.45 \\ 0.05 \\ 0.0 \\ 0.0 \end{array}$	$\begin{array}{c c} 0.44 \\ 0.75 \\ 0.33 \\ 0.20 \\ 0.12 \\ 0.10 \end{array}$	9 9 9 9 9 9 9	7 7.5 7.5 4 6 8	

^b Iodine values using the Wijs method.
 ^c Polyunsaturates by the A.O.C.S. Tentative Method Cd. 7-48.

It would quite naturally be assumed that as the refractive index and the content of polyunsaturated glycerides decreased, the flavor stability would gradually increase. Instead, in at least three cases, Series 2-4, the stability actually fell off as hydrogenation proceeded, passing through a minimum, and then rose again. Possibly soft oil reversion is not as objectionable qualitatively to panel members as that of a slightly hydrogenated oil. In any case no correlation was found between flavor stabilities and oxidative stabilities or contents of polyunsaturates.

Variation in Conditions of Hydrogenation

Experiments involving changes in hydrogenation conditions were done, using a 2-l. electrically-heated, high pressure stainless steel autoclave (Table II). The agitator was set to rotate at 520 rpm. so that the surface of the charge was almost motionless. Temperature control at high pressures and high catalyst concentration was almost impossible even at this slow rate of agitation, e.g.

To a 1500-g. sample of refined and bleached soybean oil was added 15 g. of nickel catalyst flakes. This was heated to 200°C., the heaters were shut off, and 1800 psi. of hydrogen was admitted. In 10 seconds the temperature had risen to 330° C. Then the agitator was stopped, and the converter was evacuated. The product had the following constants: R.I. (60°C.), 32.2; Titer, 64.3°C.; I. value, 6.5; FAC M.P., 154°F.

The oils prepared as described in Table II were filtered from catalyst, deodorized, and stabilized with 0.005% citric acid. Each received a flavor panel score of 9 or better when fresh. The values reported in Table II were obtained after three days' aging at 60°C.

Of samples 1, 2, and 3 from Table II, sample 3 has a melting and softening point considerably higher than would be expected on the basis of its slightly lower R.I. (0.8 unit). Apparently, relatively large quantities of high-melting glycerides form during high pressure hydrogenation. Note the improved flavor stability of 3 over 1.

Samples 4, 5, and 6 again emphasize the high melting and softening points of oil hardened at the higher pressures. The percentages of trans acids in the three samples were determined by the spectrophotometric method of Swern (6). Since the oils hardened at high pressure actually contain less of the high-melting trans acids than those hardened at low pressure, the higher melting points of the former must be due to increased amounts of fully saturated fatty acid radicals. Note also the spread between melting and softening points in the case of sample 6. Evidently products with long plastic ranges are formed during high pressure hydrogenation.

A three-fold difference in A.O.M. stabilities was found between samples 4 and 6 with almost a tenfold difference in content of linoleic acid. Yet the flavor panel actually preferred sample 6.

Sample 7 was prepared without using any added catalyst although actually traces were present in the agitator stuffing box from previous runs. The reaction chamber itself was washed free of oil and catalyst between runs. An analysis of product 7, subsequent to hydrogenation and prior to filtration, showed less than 6 parts per million of nickel to be present (a). Evidently very little active catalyst surface is necessary for hydrogenation at high pressure.

Surprisingly, these was little difference in the selectivity of hydrogenation over a wide range of temperature at 400 psi. (runs 10 and 11). Also flavor stabilities of the two oils were comparable.

Table III contains data on samples of soybean oil which were hardened in the high pressure autoclave with nickel catalyst flakes as described above. However for this series the agitator speed was increased to 1,140 rpm. This gave violent turbulence at the surface of the charge.

Samples 12-15 again illustrate the lack of correlation between flavor stability and oxidative stability. As before, the oils were graded after three days' aging at 60°C. Sample 12 was obtained by high pressure hydrogenation at a very low catalyst level. The final oil, before filtration, contained less than 6 parts per million of nickel.¹

Runs 16-20 demonstrate the effect of extreme changes in pressure on the rate and selectivity of hydrogenation. Sample 20 was obtained by bubbling hydrogen through the oil while agitating it under 20 inches of vacuum. Note that this oil is evidently higher melting than sample 19 in spite of the fact that it was hydrogenated more selectively than 19. This is probably the result of its high content of trans acids (6).

Effect of Catalyst Concentration

Samples 14 and 15 of Table III show the direct relationship which holds between catalyst concentration and selectivity at normal pressures. That is, the content of polyunsaturated glycerides at a given refractive index or iodine value varies inversely with the amount of catalyst used in the hydrogenation. Samples 23 and 24 of Table IV illustrate how this effect is reversed at high pressure.

Effect of Temperature

The change in selectivity with temperature at moderate pressure is shown by comparing samples 21 and 22 of Table IV. At 300°C. (sample 25) considerable polymerization takes place, which accounts for the

¹Spectrophotometric method, involving the development of a colored complex with dimethylglyoxime.

small drop in refractive index. Selectivity is low at this extreme temperature. Samples 10 and 11 of Table II seem to indicate that selectivity is almost independent of temperature at 400 psi.

Effect of Agitation

Samples 26 and 27 of Table IV illustrate the effect of changes in agitator speed at low pressure on chemical selectivity. At high pressure, samples 28 and 29, the effect is reversed.

Summary

No correlation was found between the flavor stability of partially hydrogenated soybean oil and its oxidative stability or its content of polyunsaturated glycerides. Fats having unusually high melting and softening points with considerable spread between melting and softening points were obtained by high pressure hydrogenation. At moderate pressures chemical selectivity was found to vary directly with catalyst concentration and inversely with agitator speed, as reported by previous workers. However at high pressures the effect of these variables was reversed. That is, selectivity then varied directly with the amount of agitation and inversely with the catalyst concentration.

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ABSTRACTS Don Whyte, Editor

Oils and Fats

R. A. Reiners, Abstractor

Reagents for idometric determination of peroxides in fats. L. Hartman and Margaret D. L. White (Dept. Sci. Ind. Res., Wellington, N. Z.). Anal. Chem. 24, 527-29(1952). It is suggested that a 10% solution of citric acid in a mixture of tert. butyl alcohol and carbon tetrachloride be used as solvent in the Lea method for peroxide determination in fats in order to reduce the blank.

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